ALLEGHENY COUNTY HEALTH DEPARTMENT AIR QUALITY PROGRAM

February 28, 2005

SUBJECT: Review of Application

Title V Operating Permit Amendment

Pittsburgh Terminals, Corp. Coraopolis Terminal

9 Thorn Street

Moon Township, PA 15108-0191

RE: Operating Permit File No. 0041a

Operating Permit Amendment for two additional roof

landings each for four gasoline and two gasoline/distillate storage tanks.

TO: Sandra L. Etzel

Chief Engineer

FROM: Erin J. O'Brian, P.E.

AMENDMENT DESCRIPTION:

This amendment is to add an additional two roof landings per tank for six gasoline and distillate/gasoline storage tanks, no.27511, 29490, 29491, 29492, 29497 & 29518. These roof landings are for RVP changes and for inspection and maintenance. The original permit did not address roof landings and no allowable emissions exist for these events. The roof landings are part of normal operation and are not a new events or new emissions. No new or increased actual or potential emissions result in this permit amendment. The allowable VOCs and HAPs from the storage tanks will be increased by 7.96 tpy and 0.43 tpy, respectively to incorporate these previously overlooked potential emissions.

AMENDED EMISSION CALCULATIONS:

Gasoline, distillate & additive tanks potential emissions:

1. VOC emissions were calculated using the US EPA TANKS 4.09b program. HAP emissions were calculated by applying the vapor weight percent to the total VOCs from each tank. Gasoline HAP vapor weight fractions are from EPA's Gasoline Distribution Industry (Stage I) – Background Information for Promulgated Standards (EPA-453/R-94-002b), Table 11.3-2. Distillate HAP estimates are from EPA's TANKS 4.09b computer program using kerosene as the stored distillate. RVP values change during the year and have been entered into the tanks program on a monthly basis. Tanks T29492 and T29518 retain the ability to store gasoline at any time therefore potential emissions for these tanks are based on gasoline. The storage of gasoline in these tanks would not have any effect on other emission sources at the facility. See Tanks 4.09b runs in operating permit amendment application 0041a.

2. Tank data and emissions: *Indicates revised estimated emissions due to updated TANKS program.

Tank no.	Size (gallons)	Max Turnovers	VOCs (tons/yr)	Contents
27511	1,705,704	86.8	4.65	gasoline*
29490	3,689,616	40.0	5.83	gasoline*
29491	3,688,566	39.0	5.83	gasoline*
29492	3,696,614	39.0	5.83	gasoline*
29497	1,693,272	85.0	3.42	gasoline*
29518	1,306,116	110.0	1.96	gasoline*
30593	2,225,454	55.0	1.03	distillate*
30594	2,225,580	55.0	1.03	distillate*

Total VOCs = 29.57 tpy

Total gasoline VOCs = 27.51 tpy, previous potential emissions were 29.00 tpy Total distillate VOCs = 2.06 tpy, previous potential emissions were 1.98 tpy

Internal Floating Roof Gasoline Storage Tanks – Working & Breathing Emissions

HAP (tons/yr)	27511	29490	29491	29492	29497	29518	Total
VOCs	4.65	5.83	5.83	5.83	3.42	1.96	27.51
2,2,4 Trimethyl- pentane	0.037	0.047	0.047	0.047	0.027	0.016	0.221
Benzene	0.042	0.052	0.052	0.052	0.031	0.018	0.247
Ethyl Benzene	0.005	0.006	0.006	0.006	0.003	0.002	0.028
Hexane	0.074	0.093	0.093	0.093	0.055	0.031	0.439
POM	0.002	0.003	0.003	0.003	0.002	0.001	0.014
Toluene	0.060	0.076	0.076	0.076	0.044	0.025	0.357
Xylenes	0.023	0.029	0.029	0.029	0.017	0.010	0.137
Total HAPs	0.244	0.306	0.306	0.306	0.179	0.103	1.444

Fixed Roof Distillate Tanks - Working & Breathing Emissions

HAP (tons/yr)	30593	30594	Total
VOCs	1.03	1.03	2.06
Benzene	0.008	0.008	0.016
Ethyl Benzene	0.021	0.021	0.042
Hexane	0.016	0.016	0.032
Toluene	0.069	0.069	0.138
Xylenes	0.043	0.043	0.086
Total HAPs	0.157	0.157	0.314

2. Tank landing emissions: due to changes in RVP tank landing must be done in tanks no.27511, 29490, 29491, 29492, 29497 & 29518 once per year. Due to maintenance and inspections an extra landing on from one to four tanks per year is required. Emissions from an additional landing for tanks 27511, 29490, 29491 & 29492, have been added to account for potential annual maintenance and inspections. See Appendix A for tank landing calculations.

Internal Floating Roof Gasoline Storage Tanks – Combined Roof Landing Emissions

Tank	TPY - VOC	TPY HAPs
27511	1.33	0.069
29490	2.35	0.124
29491	2.35	0.124
29492	2.35	0.124
29497	0.61	0.032
29518	0.46	0.024
Totals	9.45	0.497

VOC and HAP emissions from RVP landings = 5.92 tpy and 0.311 tpy VOC and HAP emissions from maintenance & inspection landings = 3.53 tpy and 0.186 tpy

AMENDED POTENTIAL EMISSIONS SUMMARY:

		ng Racks		oline ank Losses	Distillate Storage		
	& VRU		Working	Landings	Tanks	Total	
Pollutant	lbs/h r	tons/yr	tons/yr ¹ tons/yr ¹		tons/yr ¹	tons/yr1	
VOCs	39.43	32.72	27.51	9.45	2.06	71.74	
Total HAPs	2.05	1.69	1.44	0.50	0.31	3.94	

¹a year is defined as any consecutive twelve-month period

OPERATING PERMIT AMENDMENT APPLICATION COMPONENTS:

1. Amendment Application dated December 13,2004.

RECOMMENDATIONS:

The permit amendment is in compliance with all applicable regulations of Article XXI and it is recommended that the Operating Permit Amendment No. 0041a be issued.

APPENDIX A Roof Landing Emission Calculations

Coraopolis Terminal Roof Landing Emissions		T	anks 29490,	Due to Pro , 29491, 2949		ge 29497 and 29	518	
	Tank No.	29490	29491	29492	27511	29497	29518	
Roof landing date	LDATE	09/20/2004	09/20/2004	09/20/2004	09/20/2004	09/20/2004	09/20/2004	facility data
Was tank drained dry & clingage disappated ?		No	No	No	No	No	No	facility data
Take-off date	TDATE	09/23/2004	09/23/2004	09/23/2004	09/23/2004	09/23/2004	09/23/2004	facility data
Type of product or vapor in tank		Gasoline	Gasoline	Gasoline	Gasoline	Gasoline	Gasoline	facility data
Number of days tank is idle	ND	3	-3	3	3	3	3	= T _{DATE} - L _{DATE}
Tank diameter (ft)	D	120	120	120	90	80	70	facility data
Height of landed roof above tank bottom (ft)	H _{ROOF}	3.50	3.50	3.50	3.50	3.50	3.50	facility data
Effective height of stock liquid (ft)	HLE	0.00	0.00	0.00	0.00	0.00	0.00	facility data
Height of vapor space under roof (ft)	Hv	3.50	3.50	3.50	3.50	3.50	3.50	= H _{ROOF} - H _{LE}
Volume of vapor space (ft3)		39,584	39,584	39,584	22,266	17,593	13,470	$= ((H_v^*pi^*(D^*D))/4$
Vapor space expansion factor	KE	0.23	0.23	0.23	0.23	0.23	0.23	= ((DELTA T _V) / T) x ((1 + ((0.5 x B x P) / (T x (P _A - P))))
Normal height of vapor space under roof (ft)	H _{Vnorm}	0.00	0.00	0.00	0.00	0.00	0.00	facility data
Volume of vapor expelled during filling (ft3)	V _V	39,584	39,584	39,584	22,266	17,593	13,470	= (((H _V - H _{Veom})*pi*(D*D))/4
Stock liquid density (lb/gal)	W٤	6.45	6.45	6.45	6.45	6.45	6.45	facility analytical data
Reid vapor pressure (psia)	RVP	13.5	13.5	13.5	13.5	13.5	13.5	facility data
True vapor pressure of liquid (psia)	P	6.99	6.99	6.99	6.99	6.99	6.99	=EXP (A - (B /T _{LA}))
Stock vapor molecular weight (lb/lb-mole)	MW_v	61.3	61.3	61.3	61.3	61.3	61.3	est.
Ambient temp daily range (R)	DELTA TA	20.8	20.8	20.8	20.8	20.8	20.8	from TANKS program
Vapor temp daily range (R)	DELTA T_{V}	21.3	21.3	21.3	21.3	21.3	21.3	from TANKS program
Ambient temp daily avg. (F)	T _{AMB}	63.9	63.9	63.9	63.9	63.9	63.9	from TANKS program
(R)		523.6	524	523.6	523.6	523.6	523.6	from TANKS program
Liquid surface temp daily avg. (F)		58.1	58.1	58.1	58.1	58.1	58.1	from TANKS program
(R)	TLA	517.8	517.8	517.8	517.8	517.8	517.8	from TANKS program
Vapor & liquid temp. below roof - avg. (R)	Т	523.6	523.6	523.6	523.6	523.6	523.6	= T _{AMB} + 459.67
Vapor pressure equation constant "A"	Α	11.63	11.63	11.63	11.63	11.63	11.63	=15.64 - (1.854*SLOPE*0.5) - (0.8742-0.328*SLOPE*0.5) * (LN(RVP))
Vapor pressure equation constant *B*	В	5,016	5,016	5,016	5,016	5,016	5,016	= 8742 - (1042*SLOPE*0.5) - (1049-179.4*SLOPE*0.5) * (LN(RVP))
Stock ASTM-D86 distillation slope	SLOPE	3	3	3	3	3	3	from AP-42, Table 7.1-4
						-		
Atmospheric pressure (psia)	PA	14.11	14.11	14.11	14.11	14.11	14.11	from TANKS program
Ideal gas constant (psia ft3/lb-mole R)	R	10.731	10.731	10.731	10.731	10.731	10.731	
Standing idle saturation factor	Ks	0.44	0.44	0.44	0.44	0.44	0.44	= 1 / (1 + (0.053*P*H _V))
Standing idle loss per episode (lb)	Ls	916	916	916	515	407	312	= ND x K _E x (P x V _V / (R x T)) x MW _V x K _s
	L _S max	0	0	0	0	0	. 0	< 5.9 * (D*D).* H _{LE} * W _L
Loss due to clingage (drain dry only) (lb)	Ls				1			= 0.0063 W _L * pi * (D*D) / 4
						i		from Table 4 of VT-stative Mathed for Data-vision Char
Filling saturation factor	s	0.60	0.60	0.60	0.60	0.60	0.60	from Table 1 of "Tentative Method for Determining Storage Tank Evaporative Losses from Floating Roof Landings, American Petroleum Institute, January 2002"
Filling loss per episode (lb)	L _F	1,812	1,812	1,812	1,019	805	617	= (P x Vv / (R x T)) x Mv x S
Total loss per episode (lb)	L _Y	2,728	2,728	2,728	1,535	1,213	928	= L _S + L _p

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Coraopolis Terminal	1		Due to Insp	ection, Mai	ntenance,	or Emergen	су	
Roof Landing Emissions	Tanks 29490, 29491, 29492, 27511, 29497 and 29518							
	Tank No.	29490	29491	29492	27511	29497	29518	
Roof landing date	01114	09/20/2004	i			09/20/2004	09/20/2004	facility data
Was tank drained dry & clingage disappated ? Take-off date		Yes 09/23/2004	Yes	Yes 09/23/2004	Yes	Yes 09/23/2004	Yes 09/23/2004	facility data facility data
Type of product or vapor in tank	DICTE.	Gasoline	Gasoline	Gasoline	Gasoline	Gasoline	Gasoline	facility data
Number of days tank is idle.		3	3	3	3	3	3	= T _{DATE} - L _{DATE}
Tank diameter (ft) Height of landed roof above tank bottom (ft)		120 6.50	120 6.50	120 6.50	90 6.50	80 6.50	70	facility data
Effective height of stock liquid (ft)		0.00	0.00	0.00	0.00	0.00	6.50 0.00	facility data
Height of vapor space under roof (ft)		6.50	6.50	6.50	6.50	6.50	6.50	= H _{ROOF} - H _{LE}
Volume of vapor space (ft3)		73,513	73,513	73,513	41,351	32,673	25,015	= ((H ₂ *pi*(D*D))/4
Vapor space expansion factor		0.23	0.23	0.23	0.23	0.23	0.23	= $((DELTA T_V) / T) \times ((1 + ((0.5 \times B \times P) / (T \times (P_A - P)))))$
Normal height of vapor space under roof (ft)	H_{Vnorm}	0.00	0.00	0.00	0.00	0.00	0.00	facility data
Volume of vapor expelled during filling (ft3)		73,513	73,513	73,513	41,351	32,673	25,015	= (((H _V - H _{Vnorm})*pi*(D*D))/4
Stock liquid density (lb/gal)	W_L	6.45	6.45	6.45	6.45	6.45	6.45	facility analytical data
Reid vapor pressure (psia)	RVP	13.5	13.5	13.5	13.5	13.5	13.5	facility data
True vapor pressure of liquid (psia)	P	6.99	6.99	6.99	6.99	6.99	6.99	=EXP (A - (B /T _{LA}))
Stock vapor molecular weight (lb/lb-mole)	MW_{V}	61.3	61.3	61.3	61.3	61.3	61.3	est.
Ambient temp daily range (R)	DELTA T _A	20.8	20.8	20.8	20.8	20.8	20.8	from TANKS program
Vapor temp daily range (R)	DELTA T _V	21.3	21.3	21.3	21.3	21.3	21.3	from TANKS program
Ambient temp daily avg. (F)	T _{AMB}	63.9	63.9	63.9	63.9	63.9	63.9	from TANKS program
(R)		523.6	523.6	523.6	523.6	523.6	523.6	from TANKS program
Liquid surface temp daily avg. (F)	~	58.1	58.1	58.1	58.1	58.1	58.1	from TANKS program
(R)	TLA	517.8	517.8	517.8	517.8	517.8	517.8	from TANKS program
Vapor & liquid temp. below roof - avg. (R)	Т	523.6	523.6	523.6	523.6	523.6	523.6	= T _{AMB} + 459.67
Vapor pressure equation constant "A"	Α	11.63	11.63	11.63	11.63	11.63	11.63	=15.64 - (1.854*SLOPE*0.5) - (0.8742-0.328*SLOPE*0.5) * (LN(RVP))
Vapor pressure equation constant "B"	В	5,016	5,016	5,016	5,016	5,016	5,016	= 8742 - (1042*SLOPE*0.5) - (1049-179.4*SLOPE*0.5) * (LN(RVP))
Stock ASTM-D86 distillation slope	SLOPE	3	. 3	3	3	3	3 ,	from AP-42, Table 7.1-4
Atmospheric pressure (psia)	P _A	.14.11	14.11	14.11	14.11	14.11	14.11	from TANKS program
Ideal gas constant (psia ft3/lb-mole R)	R	10.731	10.731	10.731	10.731	10.731	10.731	
Standing idle saturation factor	Ks	0.29	0.29	0.29	0.29	0.29	0.29	= 1 / (1 + (0.053*P*H _V))
Standing idle loss per episode (lb)	Ls	1,147	1,147	1,147	645	510	390	= ND x K _E x (P x V _V / (R x T)) x MW _V x K _s
	L _s max	0	0	0	0	0	0 '	< 5.9 * (D*D) * H _{LE} * W _L
Loss due to clingage (drain dry only) (lb)	Ls							= 0.0063 W _L * pi * (D*D) / 4
Filling saturation factor	s	0.15	0.15	0.15	0.15	0.15		from Table 1 of "Tentative Method for Determining Storage Tank Evaporative Losses from Floating Roof Landings, American Petroleum
				l	· · ·			Institute, January 2002"
Filling loss per episode (lb)	L _F	841	841	841	473	374	286	= (P x Vv / (R x T)) x Mv x S